IN THE CLAIMS:

- 1. 2. (Cancelled).
- 3. (Currently Amended): The process according to elaim-1, Claim 15 wherein the regeneration gas may pass passes through the a catalyst bed of the second coke-burning zone in a along the centrifugal or centripetal radial direction in a centrifugal or centripetal manner, and then pass passes through a the catalyst bed of the first coke-burning zone in a centrifugal or centripetal along the radial direction in a centrifugal or centripetal manner.
- 4. (Currently Amended): The process according to elaim 1, Claim 15 wherein the regeneration gas passes may pass through a the catalyst bed of the second coke-burning zone in a centrifugal along the radial direction in a centrifugal manner, and then passes pass through a the catalyst bed of the first coke-burning zone in a centrifugal along the radial direction in a centrifugal manner.
- 5. (Currently Amended): The process according to elaim 1, Claim 15 wherein the operating pressure of the regeneration process regenerator is in the range of 0.3 0.9 MPa.
- 6. (Currently Amended): The process according to claim 1, Claim 15 wherein the water content in the regeneration gas entering the second coke-burning zone is has a water content of 10-200 ppmv.

- 7. (Currently Amended): The process according to claim 1; Claim 15 wherein the exygen content in the regeneration gas at the inlets of the first and second coke-burning zones has an exygen concentration is in the range of 0.2-1.0 v%.
- 8. (Currently Amended): The process according to elaim 1, Claim 15 wherein the temperature of the regeneration gas entering the first-coke-burning zone is at a temperature in the range of 410-480° C.
- 9. (Currently Amended): The process according to elaim 1, Claim 15 wherein the temperature of the regeneration gas entering the second coke-burning zone is at a temperature in the range of 480-520°C.
- 10. (Cancelled).
- 11. (Currently Amended): The process according to elaim 1 or 10, Claim 15 or 17 wherein said inner screen of the first coke-burning zone is may either be a cylinder with a uniform diameter, or a tapered cylinder with having a downwardly reduced diameter diameters from the top downwards.
- 12. (Currently Amended): The process according to claim 11, wherein the diameter of said inner screen may be gradually reduced is linearly reduced from its the top down with wherein its minimal diameter being is 60-90% of its maximal diameter.

13. (Currently Amended): The process according to claim 11, wherein the diameter of said inner screen is may be reduced at a the point of 40-60% from the top of the height of the first coke-burning zone in a straight down manner so that the diameter at the bottom of said inner screen is 60-90% of the diameter at the top of said inner screen.

14. (Currently Amended): The process according to claim 1 or 10, Claim 15 or 17 wherein said inner screen of the second coke-burning zone is cylindrically shaped a cylinder in shape.

15. (New): A process of continuously regenerating catalysts particles comprising passing deactivated catalyst particles downwardly, in sequence, through a first coke-burning zone, said first coke-burning zone comprising a radial bed, an inner screen and an outer screen; a second coke-burning zone, said second coke-burning zone comprising a radial bed, an inner screen and an outer screen; an oxychlorination zone and a calcination zone, wherein said deactivated catalyst particles are contacted in said first coke-burning zone with regeneration gas from said second coke-burning zone, supplementary dry air and an inert gas; said regeneration gas being withdrawn from said first coke-burning zone and recycled back into said second coke-burning zone where it is contacted with said catalyst particles previously contacted in said first coke-burning zone.

16. (New): The process according to Claim 15 wherein said regeneration gas is dried after being withdrawn from said first coke-burning zone before being recycled into said second coke-burning zone.

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17. (New): A process of continuously regenerating catalyst particles comprising passing deactivated catalyst particles from moving bed reactors downwardly by gravity, in sequence, through a first coke-burning zone, said first coke-burning zone comprising a radial bed, an inner screen and an outer screen; a second coke-burning zone, said second coke-burning zone comprising a radial bed, an inner screen and an outer screen; an oxychlorination zone; and a calcination zone wherein a dry oxygen-containing gas at a temperature in the range of . between 480°C and 520°C is introduced into the bottom of said second coke-burning zone; passing said gas through a catalyst bed of said second coke-burning zone in a centrifugal or centripetal radial direction wherein coke present on said catalyst particles are burned off; cooling said gas from said second coke-burning zone to a temperature in the range of 410°C to 480°C by adding dry air and a dry inert gas; introducing said gas, passed through said second coke-burning zone, into said first coke-burning zone; passing said gas through a catalyst bed of said first coke-burning zone in a centrifugal or centripetal radial direction wherein coke is burned off said catalyst particles; withdrawing said gas from said first cokeburning zone; mixing said withdrawn gas with outlet gas from said oxychlorination zone; drying said gas in a recovery system wherein said gas is dried; passing said dry gas through a compressor, heating said compressed dry gas to a temperature in a range of 480°C to 520°C; and recycling said heated compressed dry gas to said second coke-burning zone wherein said recycled gas enters said first and said second coke-burning zone having an oxygen concentration in a range of 0.2 to 1.0 v%; and wherein said recycled gas enters said second coke-burning zone having a water concentration of 10 to 200 ppmv, said process occurring at an operating pressure in the range of 0.3 MPa to 0.9 MPa.